

Fast preconditioned solution of Navier-Stokes equations for compressible flows with physics

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Jameson 80th Birthday

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Lecture outline

RK/Implicit smoother scheme

Turbulent models

Low Mach flows

Time dependent - Dual time step

Real gas equation of state

Chemical reactions source terms

Two-phase flow

Results

Conclusions



Why Accelerate

- Complicated multiple industrial applications
- Dual time step
- Multiple trial runs to improve accuracy

(partial) **History**

- JST
- Jameson multigrid
- Jameson Implicit Residual Smoothing
- Jameson & Caughey
- Rossow , Swanson & Turkel
- High order accurate schemes (?)

Navier-Stokes Equations

The Navier-Stokes equations for the conservative variables:

$$Q = \left\{ \rho_1 \quad \rho_2 \quad \dots \quad \rho_n \quad \rho u \quad \rho v \quad \rho w \quad \rho e \right\}^T ; \quad \rho = \sum_{i=1}^n \rho_i$$

N-S equations in conservative form:

$$\frac{\partial Q}{\partial t} + \frac{\partial (F - F_V)}{\partial x} + \frac{\partial (G - G_V)}{\partial y} + \frac{\partial (H - H_V)}{\partial z} = S$$

- F , G and H are the inviscid fluxes
- F_V , G_V and H_V are the viscous fluxes

$$F \cdot \vec{n} = \begin{pmatrix} \rho_1 (\vec{V} \cdot \vec{n}) \\ \vdots \\ \rho_N (\vec{V} \cdot \vec{n}) \\ \rho u (\vec{V} \cdot \vec{n}) + n_x P \\ \rho v (\vec{V} \cdot \vec{n}) + n_y P \\ \rho w (\vec{V} \cdot \vec{n}) + n_z P \\ (E + P)(\vec{V} \cdot \vec{n}) \end{pmatrix} \quad F_v \cdot \vec{n} = \begin{pmatrix} -\rho_1 \vec{v}_1 \cdot \vec{n} \\ \vdots \\ -\rho_N \vec{v}_N \cdot \vec{n} \\ \tau_x \cdot \vec{n} \\ \tau_x \cdot \vec{n} \\ \tau_x \cdot \vec{n} \\ (-q_x + \tau_x V - \sum_{k=1}^N \rho_k \vec{v}_k h_k) \cdot \vec{n} \end{pmatrix} \quad S = \begin{pmatrix} \dot{\rho}_1 \\ \vdots \\ \dot{\rho}_n \\ 0 \\ 0 \\ 0 \\ 0 \end{pmatrix}$$

$$E = \rho \left(\frac{P}{(\gamma - 1)\rho} + \frac{1}{2} u^2 \right) \quad \text{for ideal gas} \quad E = \sum_{k=1}^N \rho_k e_k(T) + \rho \frac{1}{2} u^2 \quad \text{for a real gas}$$

\vec{v}_j are the diffusion velocities of the species j

h_j are the specific enthalpy per unit mass of the species j

τ_x is the stress tensor and q is the heat flux

P is the pressure and V is the velocity of the gas

RK/Implicit smoother with source terms

The equations set we solve in conservative form is:

$$\frac{\partial Q}{\partial t} + \nabla F = S(Q)$$

Applying the Gauss theorem for an arbitrary control volume and discretization in time yields the basic scheme:

$$\frac{\Delta Q}{\Delta \tau} = S - \frac{1}{V} \oint_S F \cdot \vec{n} ds = S - \frac{1}{V} \sum_{\text{all faces}} F \cdot \vec{n} ds$$

The Runge-Kutta time marching scheme is:

$$Q^{k+1} = Q^0 - \alpha_k \Delta t R^k$$

The residual of the k-th step is:

$$R^k = S^k - \frac{1}{V} \sum_{all\ faces} F^k \cdot \vec{n} ds$$

For accelerating the calculations using large CFL numbers the residual is replaced by a spatially smoothed residual \tilde{R}^k

Following Rossow 2006, Swanson et al. 2007,
we start with the spatially discretized equation:

$$\frac{\Delta Q}{\Delta t} + \frac{1}{V} \sum_{\text{all faces}} F \cdot \vec{n} ds - S = 0$$

Linearizing F and S in time we obtain:

$$\left(I + \frac{\Delta t}{V} \sum_{\text{all faces}} A \cdot \vec{n} ds - \Delta t \frac{\partial S}{\partial Q} \right) \Delta Q = R^k$$

$$A \equiv \frac{\partial F}{\partial Q} \quad \text{- the flux Jacobian}$$

$$\frac{\partial S}{\partial Q} \quad \text{- the source Jacobian}$$

Transforming the equations to primitive variables, the flux Jacobian is written as:

$$A = A^+ + A^-$$

where

$$A^\pm = \frac{1}{2} (A \pm |A|)$$

Finally, the implicit smoothing scheme is given by:

$$\begin{aligned} & \left(I + \varepsilon \frac{\Delta \tau}{Vol} \sum_{all\ faces} A^+ \vec{n} dS - \varepsilon \Delta \tau \frac{\partial S}{\partial Q} \right) \Delta \tilde{Q}_{local} \\ & = R^k - \varepsilon \Delta \tau \sum_{all\ faces} A^- \Delta \tilde{Q}_{NB} \vec{n} dS \end{aligned}$$

➤ **k- ω SST model equations - nonconservative**

$$\frac{\partial k}{\partial t} + \vec{u} \cdot \nabla k = P_k - \beta^* k \omega + \frac{\partial}{\partial x_j} \left[(\nu + \sigma_k \nu_T) \frac{\partial k}{\partial x_j} \right]$$

$$\frac{\partial \omega}{\partial t} + \vec{u} \cdot \nabla \omega = \alpha S^2 - \beta \omega^2 + \frac{\partial}{\partial x_j} \left[(\nu + \sigma_\omega \nu_T) \frac{\partial \omega}{\partial x_j} \right] + 2(1 - F_1) \sigma_{\omega 2} \frac{1}{\omega} \frac{\partial k}{\partial x_j} \frac{\partial \omega}{\partial x_j}$$

➤ **Spalart-Allmaras model equation - nonconservative**

$$\frac{\partial \tilde{\nu}}{\partial t} + \vec{u} \cdot \nabla \tilde{\nu} = C_{b1} (1 - f_{t2}) \tilde{S} \tilde{\nu} + \frac{1}{\sigma} \left\{ \nabla \left[(\nu + \tilde{\nu}) \nabla \tilde{\nu} + C_{b2} |\nabla \tilde{\nu}|^2 \right] \right\} - \left[C_{w1} f_w - \frac{C_{b1}}{\kappa^2} f_{t2} \right] \left(\frac{\tilde{\nu}}{d} \right)^2$$

Low speed artificial flux:

$$f_{i+1/2} = \frac{1}{2} A \cdot (u_{i+1} + u_i) - \frac{1}{2} |A| \cdot (u_{i+1} - u_i)$$

where $|A| = |A|(c')$

$$c' = \sqrt{\alpha^2 q^2 + M_r^2 c^2} \quad \alpha = \frac{1}{2} (1 - M_r^2)$$

$$M_r^2 = \min \left(\max \left(M^2, kM_\infty^2 \right), 1 \right)$$

and in the RK implicit smoother operator

$$R = R(c')$$

Time dependent - Dual time step

- For steady state use pseudo time approach
- Dual time stepping used for time dependent flow to use acceleration methods developed for steady state flow
- Physical time derivative is source term in equations
- Approximate physical time derivative with a backward difference scheme:

$$\frac{\partial Q}{\partial t} \approx \frac{3Q^{n+1} - 4Q^n + Q^{n-1}}{2\Delta t}$$

Since we do not know Q^{n+1} we approximate by with Q^k . The residual is now

$$R^k = \nabla F + \frac{3Q^k - 4Q^n + Q^{n-1}}{2\Delta t}$$

For dual time steps the smoothing operator is slightly modified:

$$\left(I + \varepsilon \frac{\Delta t}{Vol} \sum_{all\ faces} A^+ \vec{n} dS + c_t \alpha_k \frac{\Delta \tau}{\Delta t} I \right) \Delta \tilde{Q}_{local}$$

$$= R^k - \varepsilon \Delta t \sum_{all\ faces} A^- \Delta \tilde{Q}_{NB} \vec{n} dS$$

Real gas equation of state

The equation of state is:
$$P = \frac{\rho RT}{W} = RT \sum_{i=1}^n \omega_i$$

ω_k, w_k - Molar concentration and molecular weight of the species

The mean molecular weight is:
$$W^{-1} = \sum_{i=1}^n \frac{\rho_i}{\rho} \frac{1}{w_i}$$

The mean internal energy per unit mass is:

$$e(T) = \sum_{i=1}^N y_i e_i(T)$$

Chemical reactions source terms – Arrhenius model

The source term vector, S , describes the rate of change of species k :

$$\dot{\rho}_k = \frac{d\rho_k}{dt} = w_k \dot{\omega}_k \quad \dot{\omega}_k = \sum_{i \in \text{all reactions}} \nu_{ik} q_i \quad k = 1, 2, \dots, N$$

- ω_k , w_k - Molar concentration and molecular weight of the species
- ν_{ik} - Stoichiometric coefficients of the species k in the reaction i
- q_i - The rate of progress variables given by - $q_i = q_{f,i} - q_{r,i}$

$q_{f,i}$ and $q_{r,i}$ are defined by:

$$q_{f,i} \equiv k_{f,i} \prod_{k \text{ species}} \omega_k^{\nu'_{ki}} \quad ; \quad q_{r,i} \equiv k_{r,i} \prod_{k \text{ species}} \omega_k^{\nu''_{ki}}$$

The forward reaction rate k_f and the reverse rate k_r are empirically known functions of the temperature.

The forward constant is given by an Arrhenius expression of the type:

$$k_{f,i} = A_i T^{\beta_i} e^{-E_i / RT} \quad k_{r,i} = K_p \left(\frac{P_{atm}}{RT} \right)^{\sum_{k \in K_i} \nu_{ik}} \quad K_p = \exp \left(\frac{\Delta S}{R} - \frac{\Delta H}{RT} \right)$$

- A_i , β_i and E_i are the Arrhenius constants:
- A_i is the rate constant
- β_i is the temperature exponent
- E_i is the activation energy.

The source term for the temperature is

$$\dot{T} = -\frac{1}{\rho c_v} \sum_k h_k \dot{\rho}_k$$

Two-phase flow

- Solution of reactive, turbulent two-phase flow
- Gaseous main phase
- Continuous dispersed phase includes mixture of liquid and solid particles
- Particles void fraction is negligible

Coupled Navier-Stokes and dispersed phase system

In N-S equations a source term due to the dispersal phase is added

$$\frac{\partial Q}{\partial t} + \frac{\partial(F - F_V)}{\partial x} + \frac{\partial(G - G_V)}{\partial y} + \frac{\partial(H - H_V)}{\partial z} = -S_f$$

The EDP equation model – “fluidized” equation for the dispersed phase

The variables we solve for are $\{\rho_p, \vec{v}_p, T_p, \chi_p\}^T$

ρ_p, \vec{v}_p, T_p are the dispersed phase density, velocity and temperature

χ_p is the solid fraction $0 \leq \chi_p \leq 1$

when $\chi_p = 1$ the particles are totally solid,

when it's equal to zero, the particles are liquid.

Conservation of mass $\frac{\partial \rho_p}{\partial t} + \nabla(\rho_p \vec{v}_p) = 0$

Momentum $\left(\frac{\partial v_{p,i}}{\partial t} + \vec{v}_p \cdot \nabla v_{p,i} \right) = \frac{f_D}{\tau_u} \cdot (v_{g,i} - v_{p,i}) \quad ; i = (x, y, z)$

Temperature $\frac{\partial T_p}{\partial t} + \vec{v}_p \cdot \nabla T_p = \begin{cases} \frac{\dot{Q}}{m_p C_{p,p}} & T \neq T_{melt} \\ 0 & \text{otherwise} \end{cases}$

where $\dot{Q} = m_p C_{p,p} \frac{f_N}{\tau_T} (T_f - T_p)$

Solid fraction $\frac{\partial \chi_p}{\partial t} + \vec{v}_p \cdot \nabla \chi_p = \begin{cases} -\frac{\dot{Q}}{m_p L_m} & T = T_{melt} \\ 0 & \text{otherwise} \end{cases}$

The source terms for the N-S EDP equations are

$$\vec{S}_f^{cons} = \begin{pmatrix} 0 \\ -\frac{f_D}{\tau_u} \rho_p (u_f - u_p) \\ -\rho_p \frac{f_D}{\tau_u} (v_f - v_p) \\ -\rho_p \frac{f_D}{\tau_u} (w_f - w_p) \\ -\rho_p C_{p,p} \frac{f_N}{\tau_T} (T_f - T_p) - \frac{f_D}{\tau_u} \rho_p \vec{u}_p \cdot (\vec{u}_f - \vec{u}_p) \end{pmatrix}$$

where

$$F_D = \begin{cases} 1 + 0.15 \text{Re}_p^{0.687} & \text{Re}_p < 1000 \\ 0.01833 \text{Re}_p & \textit{else} \end{cases} ; \quad F_N = 1 + 0.3 \text{Re}_p^{0.5} P_r^{0.33}$$

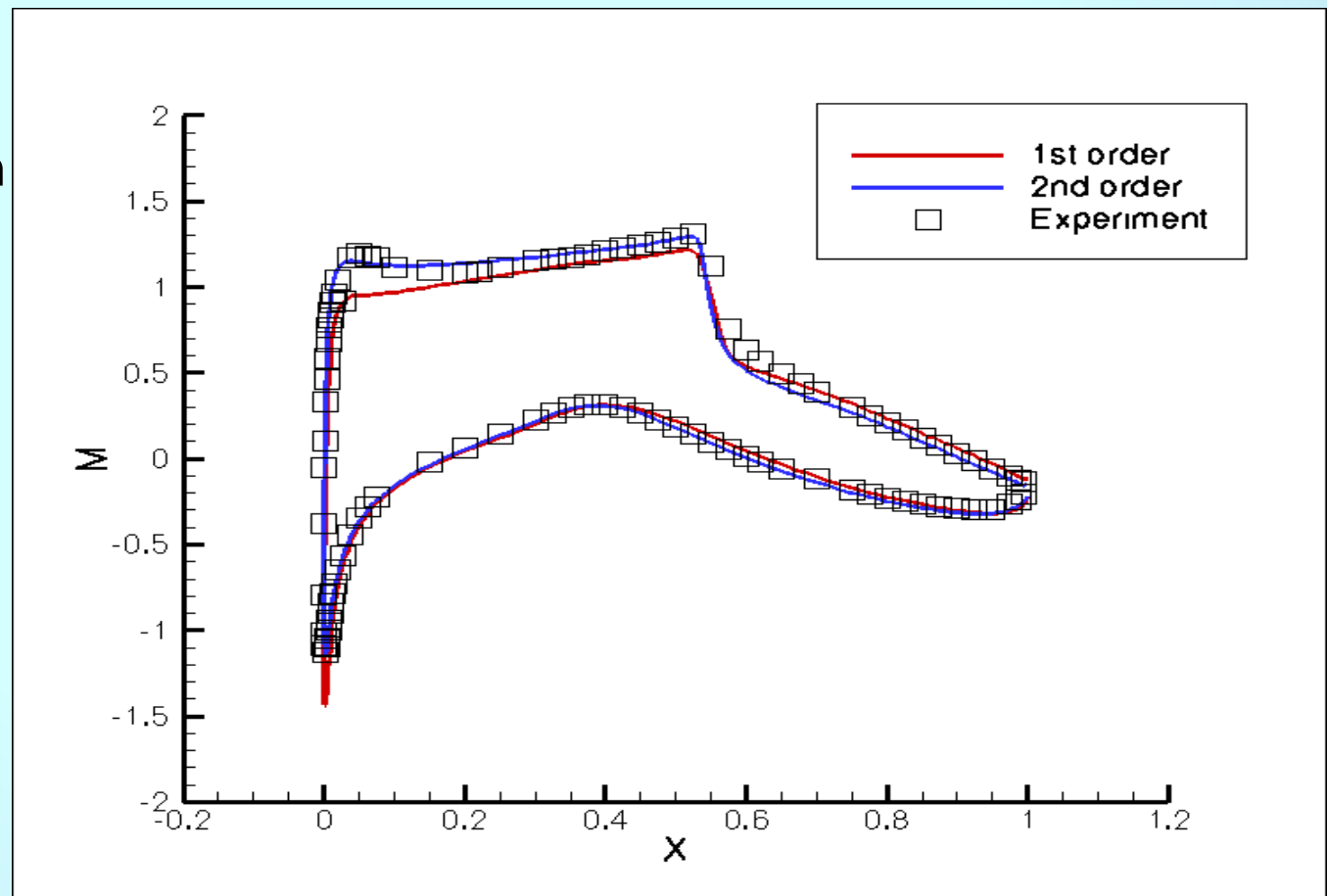
Results

- Turbulent flow – Transonic flow over RAE 2822 airfoil
- Turbulent reactive flow – rocket motor plume
- Time dependent - high angle of attack over NACA0012
- Low Mach Flow
- Two phase flow inside ballistic evaluation motor
- Conjugate heat transfer flow in converging-diverging nozzle

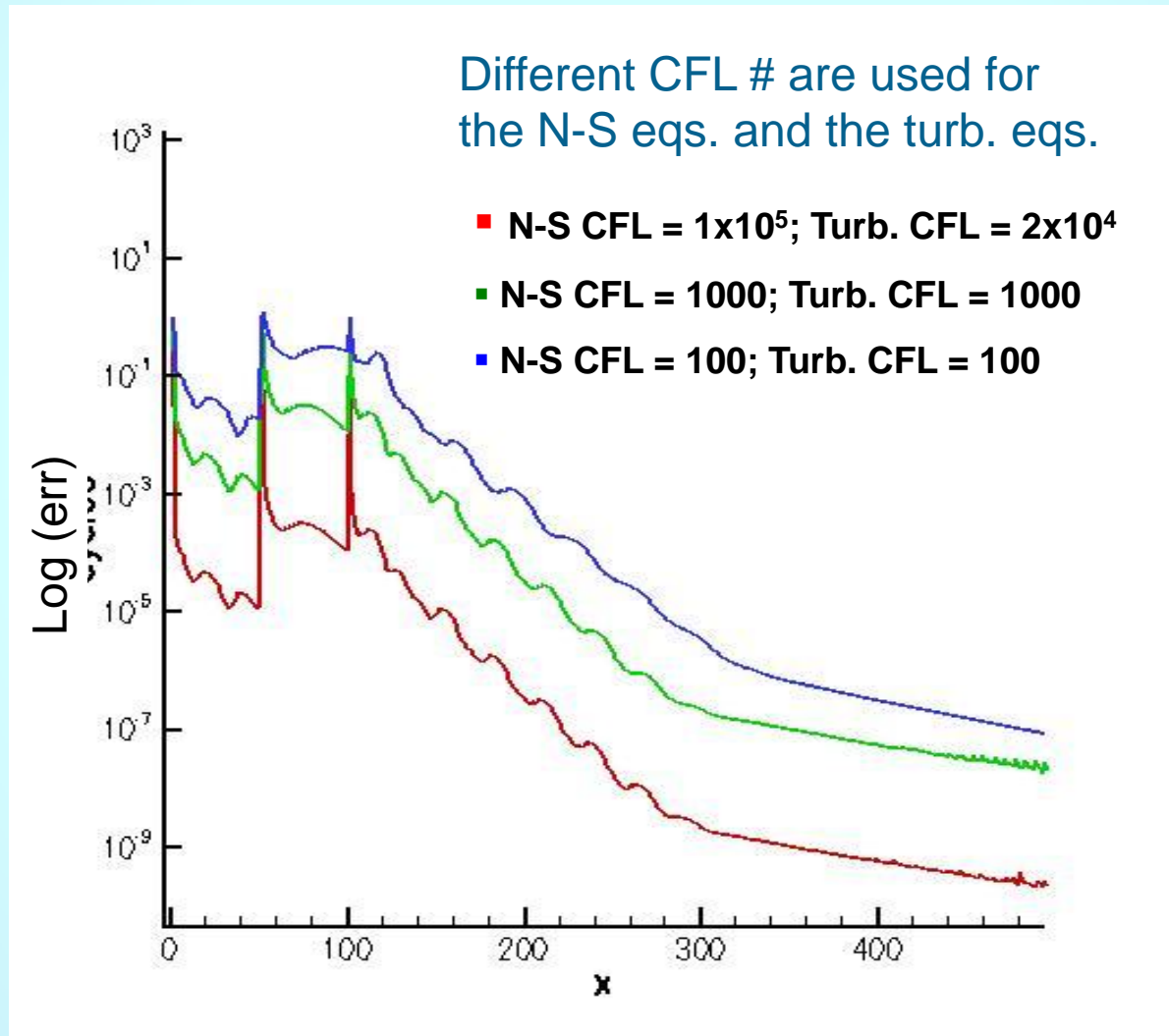
SST Turbulent flow – Transonic flow over RAE 2822 airfoil

$$M = 0.73 \quad \alpha = 2.79^\circ \quad Re \sim 17 \times 10^6$$

Comparison between experimental and computational pressure coefficient - C_p



Convergence History for Various CFL Numbers

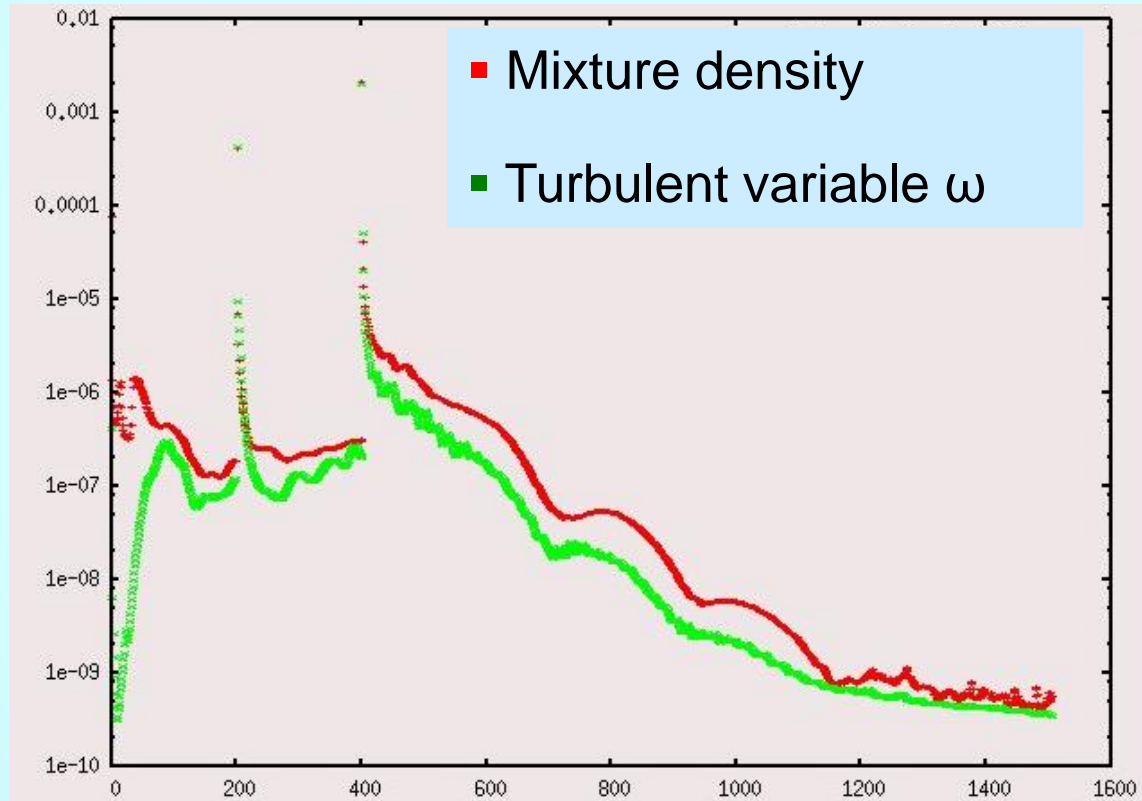


Turbulent reactive flow – rocket motor plume

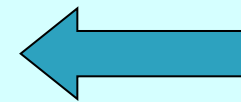
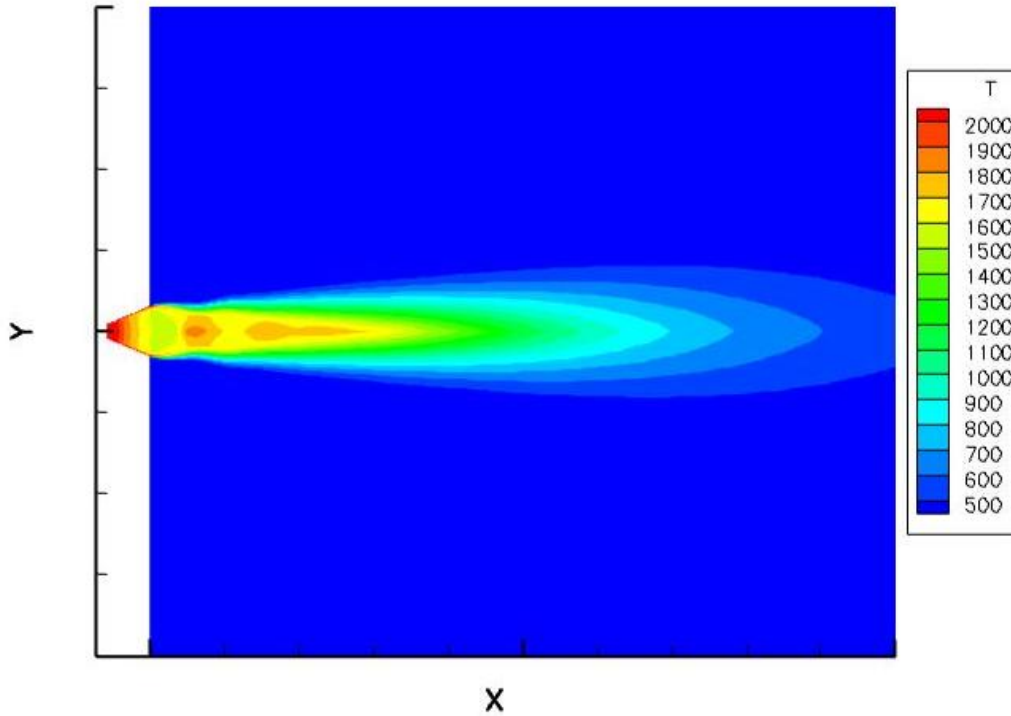
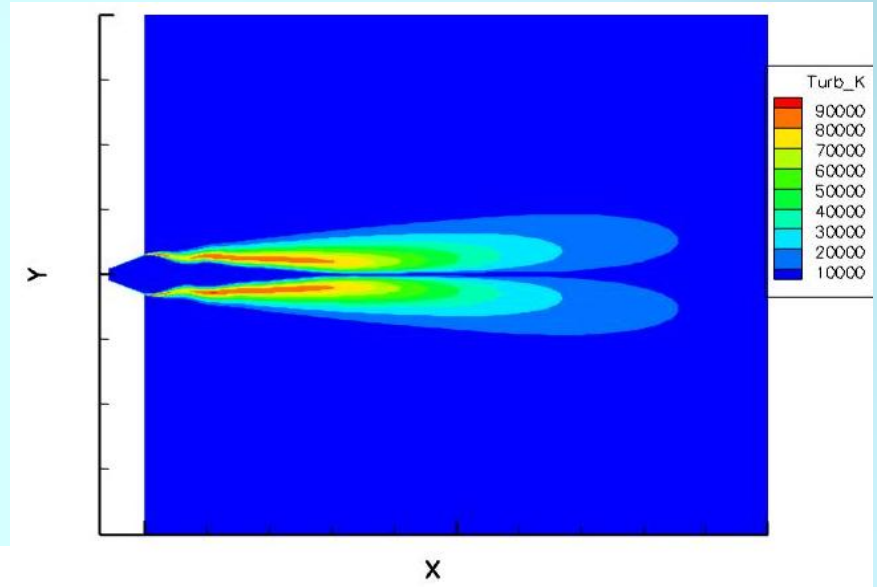
- A rocket motor plume exiting from the motor nozzle into a low Mach number free stream flow.
- The flow velocity on the nozzle throat is sonic and the species mass fractions are defined.
- The species used for this problem are: H, O, OH, H₂, O₂, CO, CO₂, H₂O, HCl and N₂.
- About 50 chemical reactions were considered

Convergence history

fluid CFL =100,000 and turbulent CFL =200

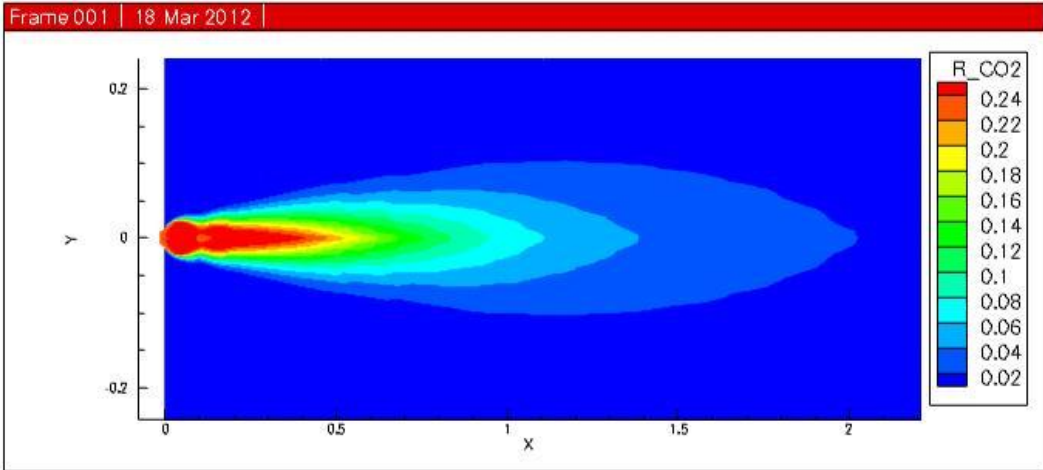


Turbulent kinetic energy

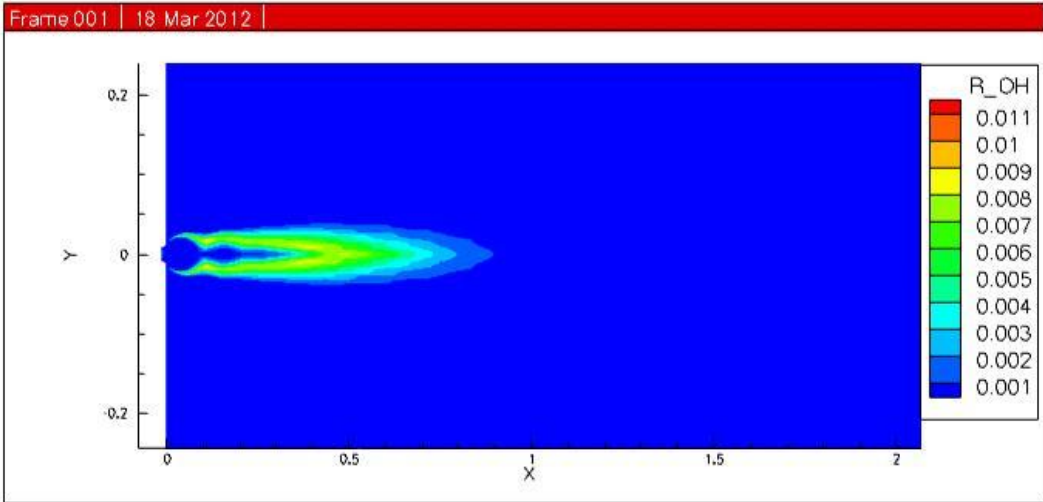


Temperature

CO2 mass fraction (A) and OH radical (B)



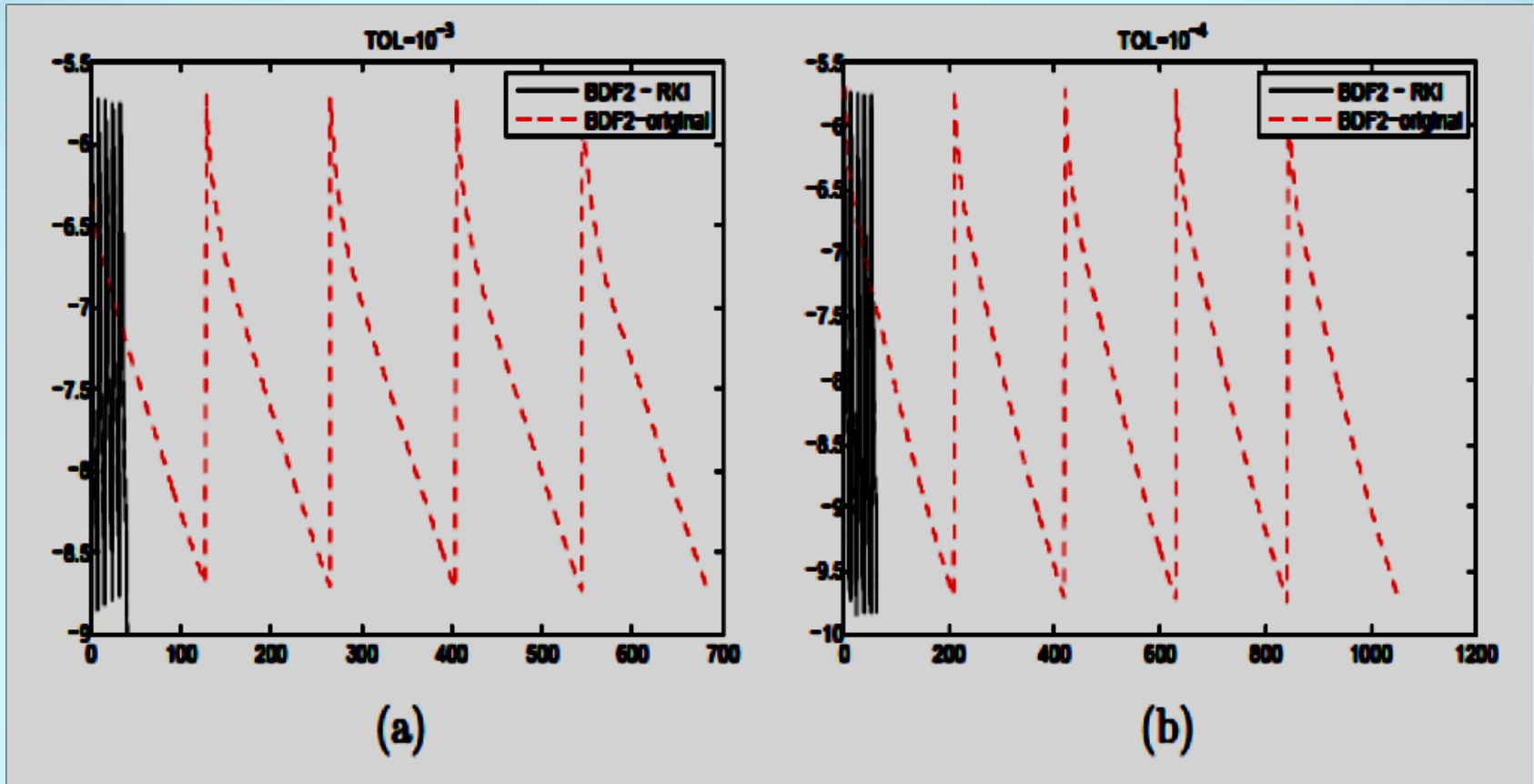
A



B

Dual time step for flow over NACA0012

- $M_\infty=0.1$, angle of attack = 30° , $Re = 3 \times 10^6$
- 150 physical time steps. $\Delta t_{\text{physical}} = 0.2 \text{ sec.}$
- CFL = 100, relaxation factor $\varepsilon = 0.5$



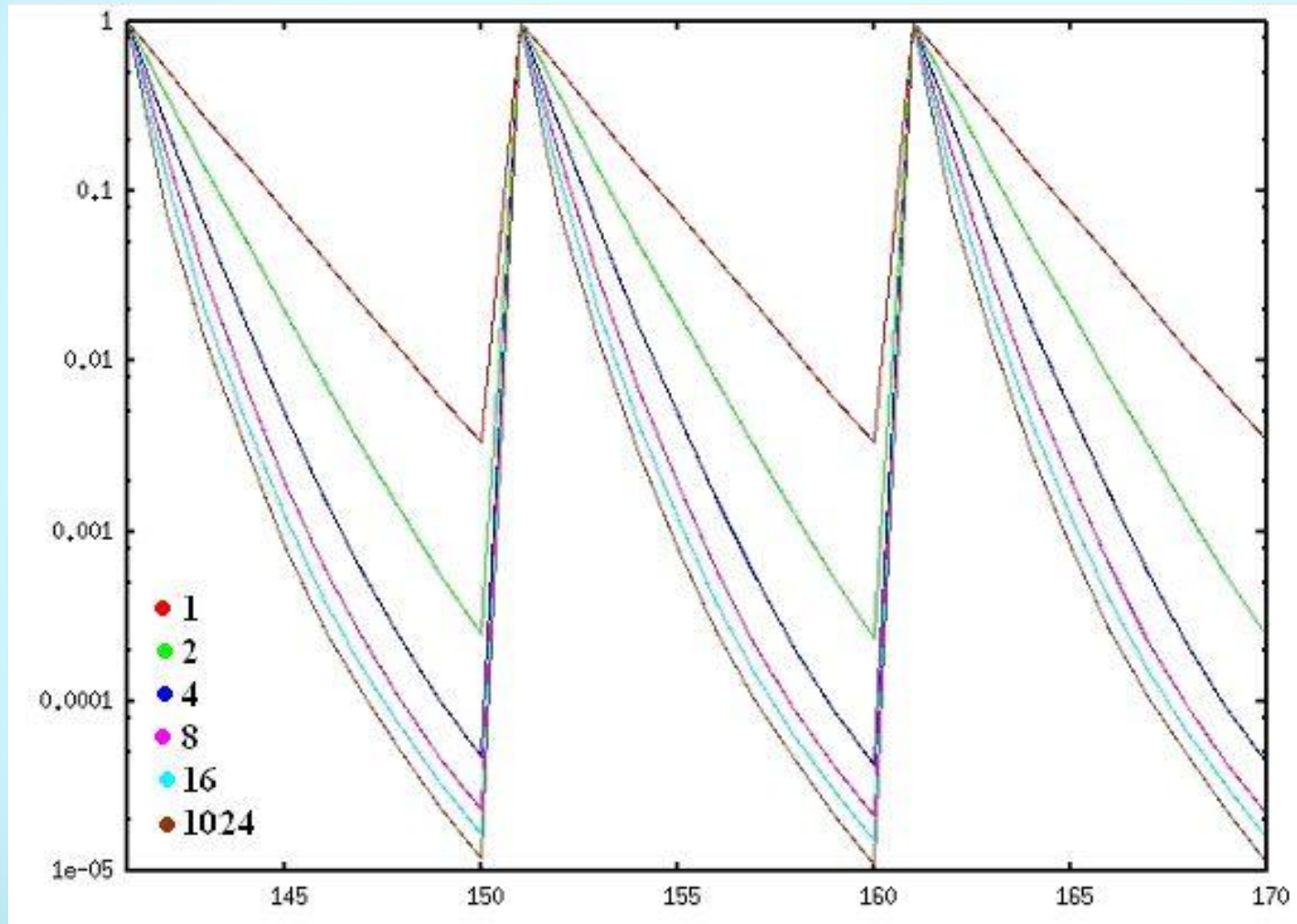
Residual reduced 3 orders

Residual reduced 4 orders

In summary: the smoothed dual time step code needs only about 10% of the CPU time of the original code.

Convergence history for series of CFL numbers

Time Dependent Riemann problem



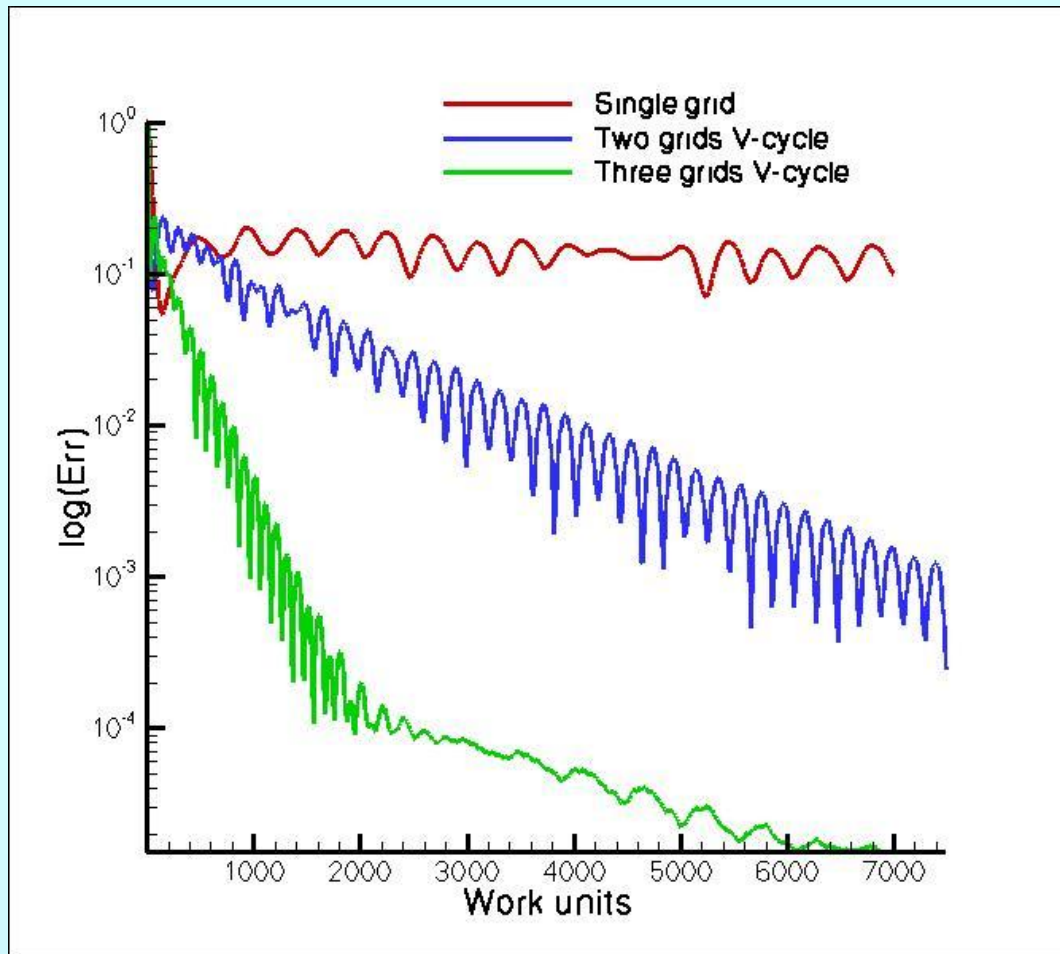
Efficiency of MG for dual time steps

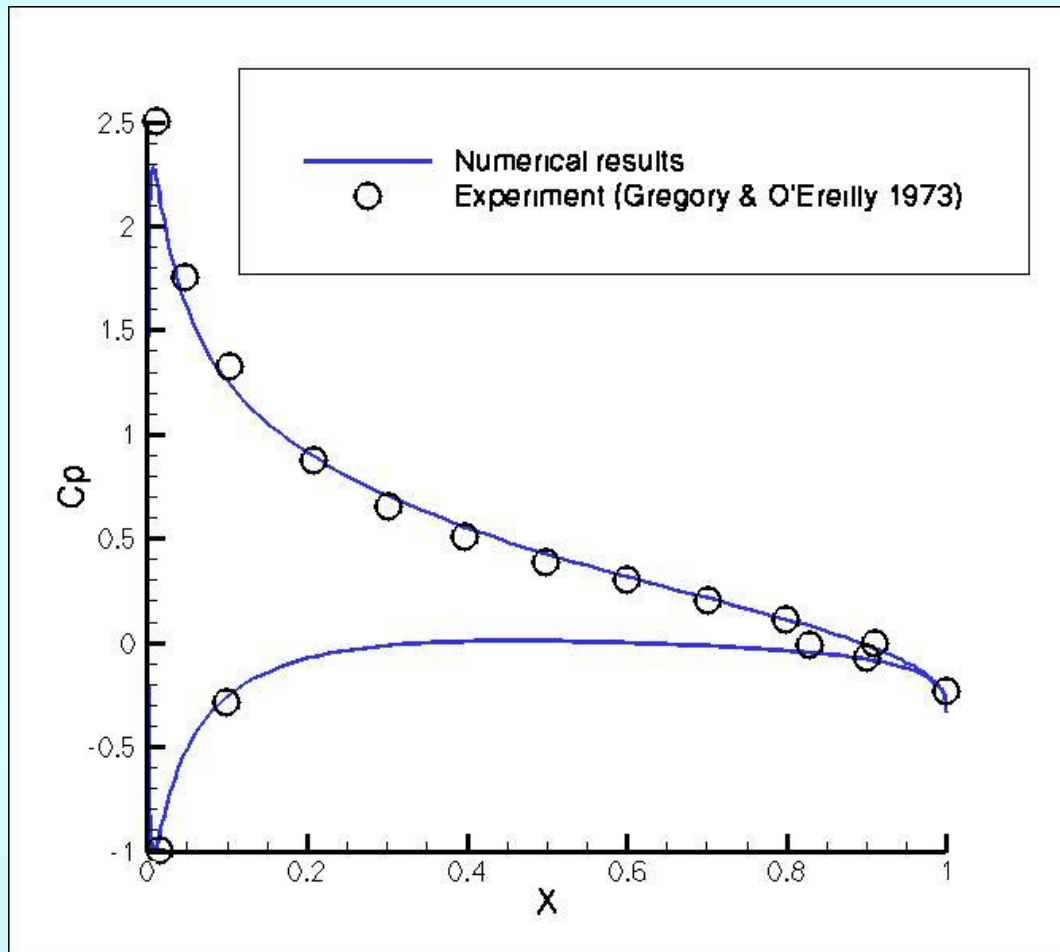
Depends on Δt

| | TOL= 10^{-3} | | TOL= 10^{-4} | |
|-------------|--------------------|---------------|--------------------|---------------|
| # MG levels | Avg # subiteration | CPU | Avg # subiteration | CPU |
| no MG | 14.56 | 12 min 8 sec | Δt 23.93 | 19 min 58 sec |
| 2 | 9.79 | 11min 51 sec | 16.97 | 20 min 22 sec |
| 3 | 9.22 | 11 min 3 sec | 16.29 | 20 min 2 sec |
| 4 | 8.98 | 12 min 17 sec | 16.23 | 19 min 16 sec |

Low Mach Flows

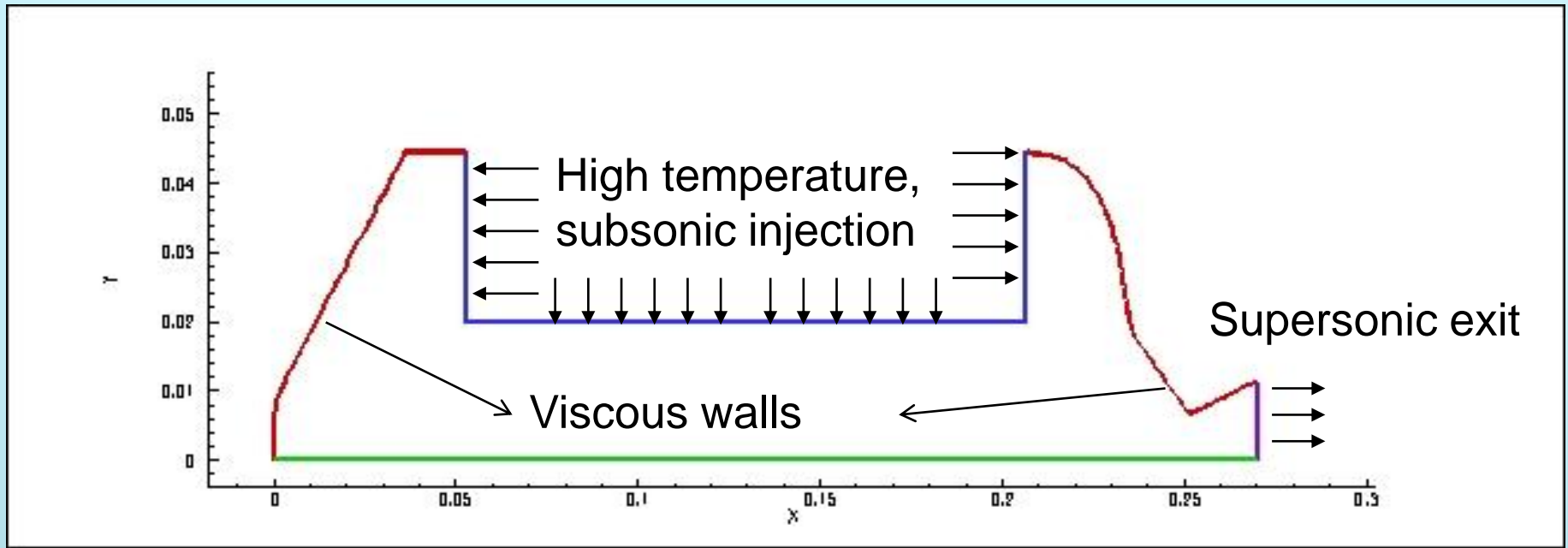
NACA0012 $M=0.001$



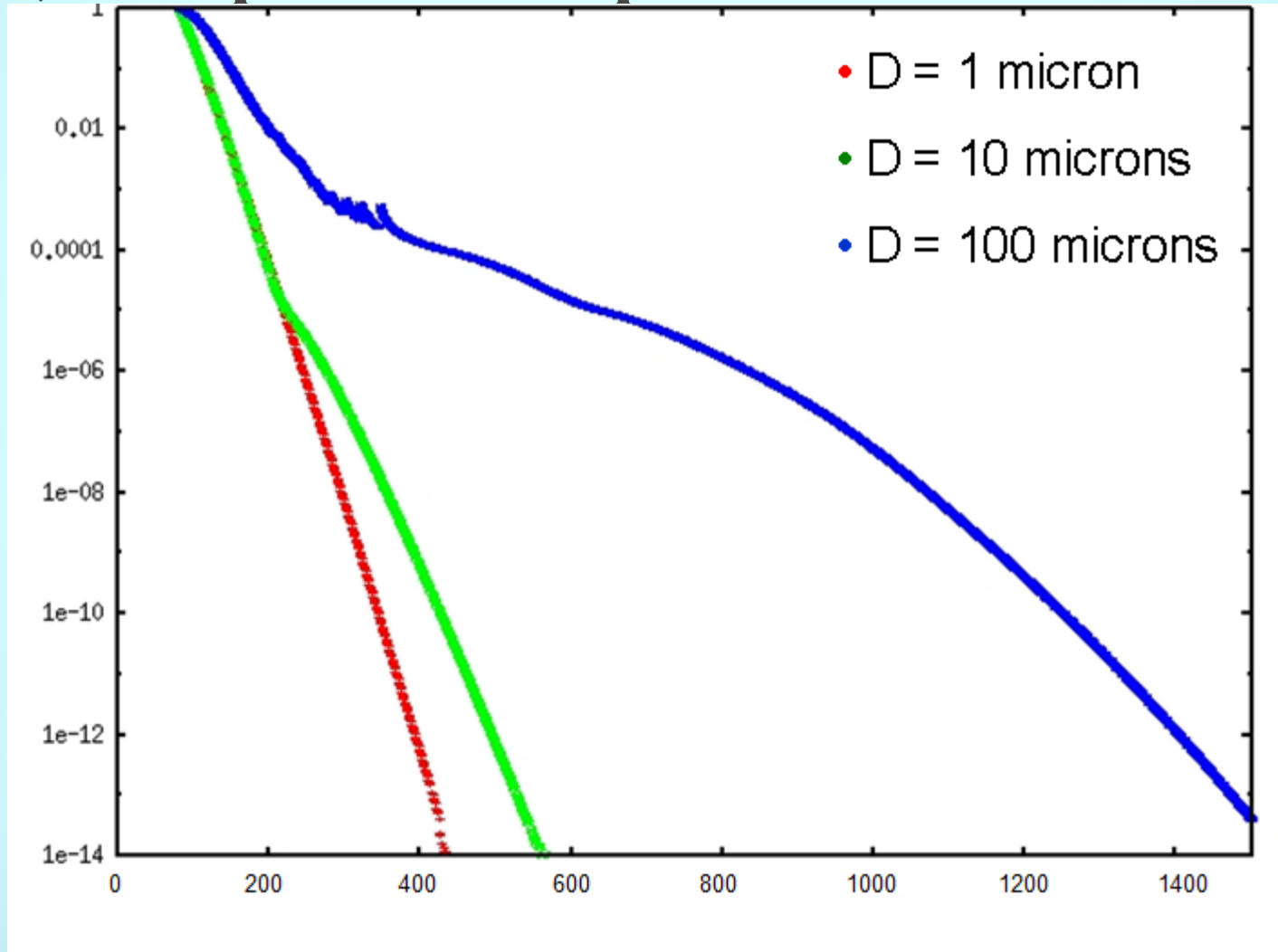


Evaluation Motor (BEM)- EDP

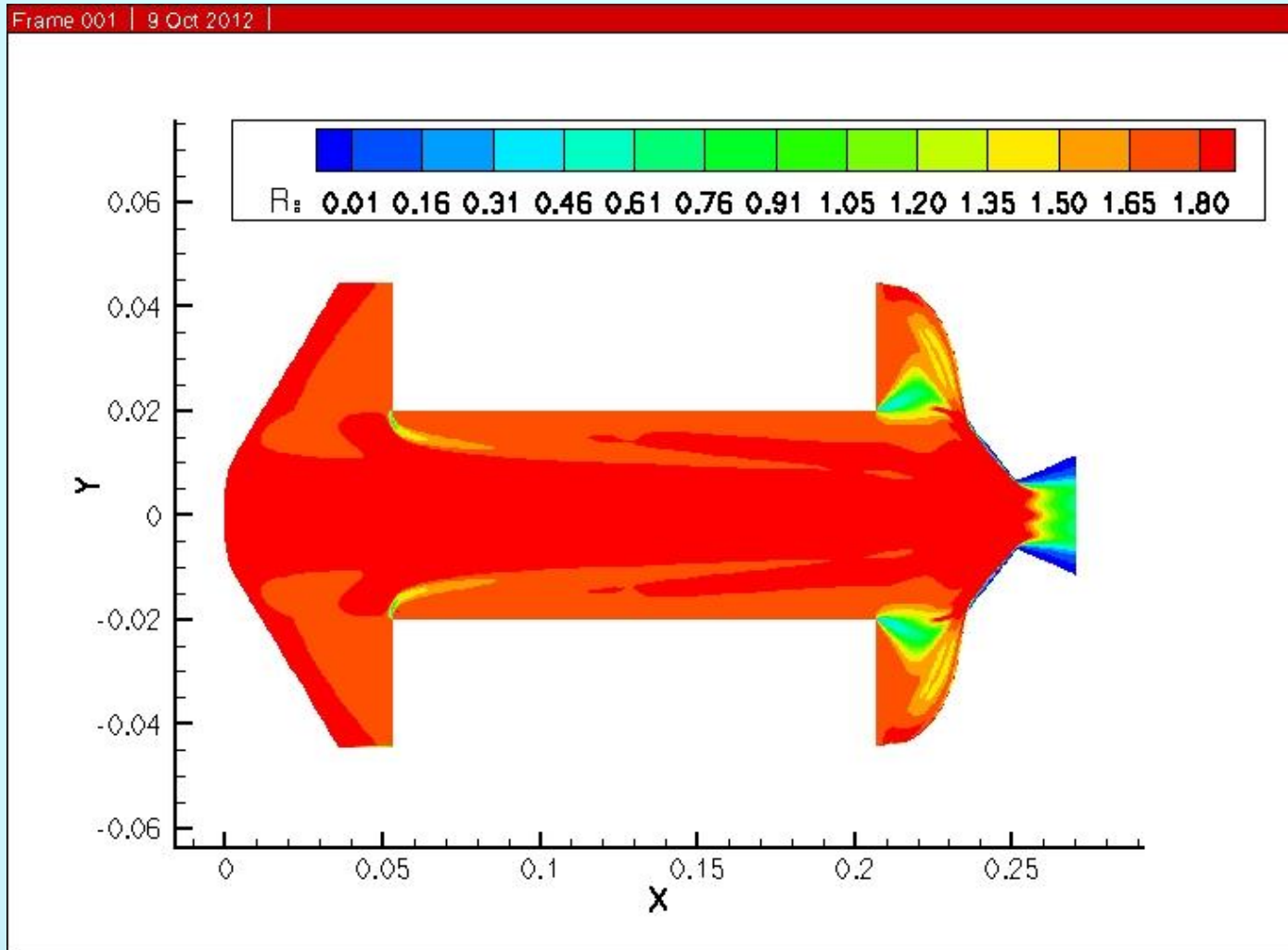
- The problem of flow inside a solid rocket motor is solved using:
- Finite volume, local time step, 3 levels sequencing and multigrid acceleration
- The schemes that were used are first order upwind for the EDP system and AUSM+UP for the gas phase system



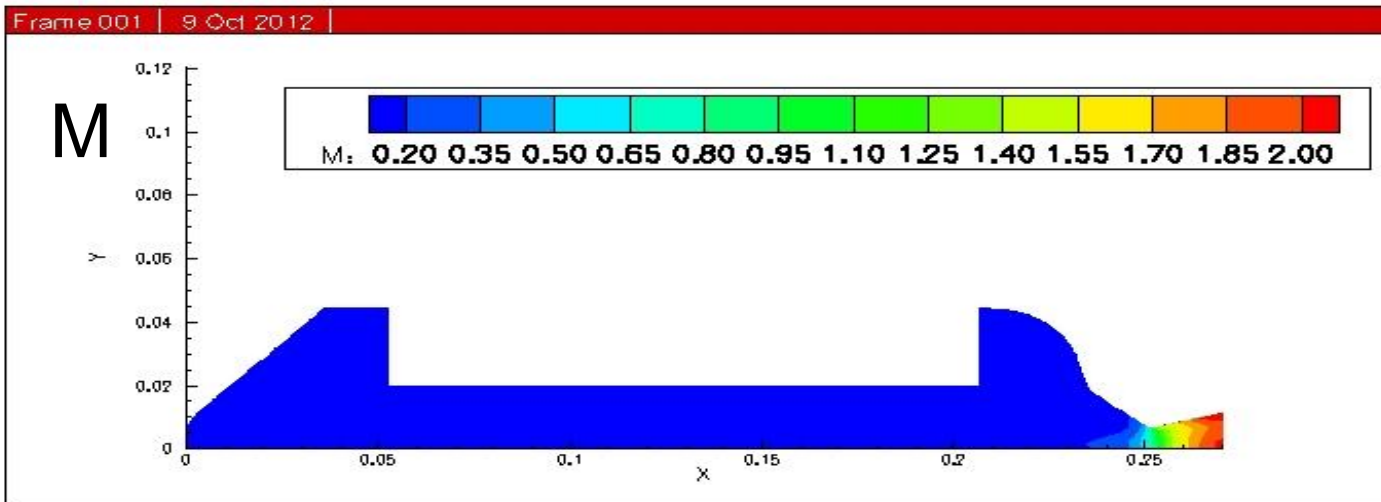
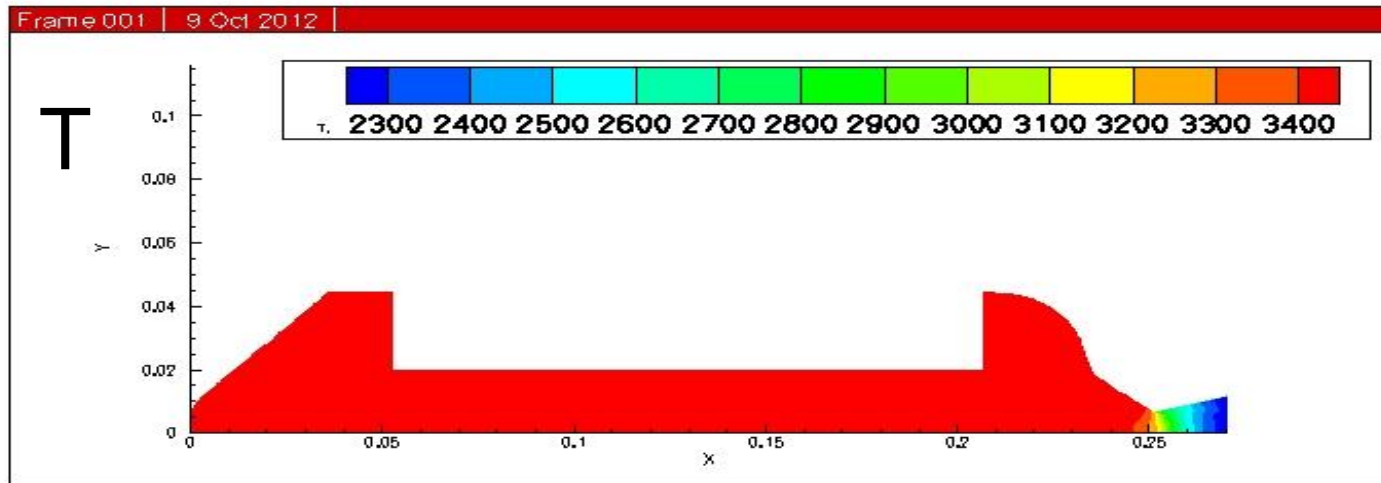
Typical convergence history (Dispersed phased density)



Global view of contour map for disperse phase density (5 microns)



Typical contour map for gas phase temperature and Mach number



Conclusions

- RK/implicit smoothing allows larger time step
- The smoother allows faster convergence of complex and stiff flow problems including turbulent reactive flow
- Reactive flow equations are solved without operator splitting
- Two Phase Flow
- Faster convergence in sub-iterations of dual time step
- Low Mach $M=0.001$ solved
- More robust solutions